

Odour Problem and Cost-Effective Solution in Sewerage Industry

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Abstract : *Odour Problems have become an environmental issue with increasing populations and decreasing buffer boundaries resulting in much friction between firms and the local population. Today, the knowledgeable general public demands effective control and treatment of odour emissions from sewage handling, and treatment facilities. Installed Odour Control Systems must be cost efficient and sustainable long term.*

This Paper is on a specific Case Study of an Odour Control and Treatment System carried out in year 2010 for a Sewage Pumping Station with gaseous emissions of very high odour levels and dangerous Hydrogen Sulphide (H₂S) concentration unlike most other typical Sewage Pumping Stations. This Case Study will illustrate the required Accurate Odour Problem Definition of identifying the odour sources, their containment with practical covers/enclosures and local exhaust to maintain negative containment, followed by the Cost-effective Odour Treatment of the exhaust odorous gases before final emission to the atmosphere.

The findings confirm very high and dangerous H₂S levels among other odorous constituents in the incoming sewage. The results show clearly that combined Odour Treatment Technologies can effectively reduce the final treated odour level to below 1,000 OU/cu.m in compliance to the requirements of the Sewage Pumping Station Owner.

Key words: *accurate odour problem definition, odour concentration, odour control system, containment system, cost-effective odour treatment*

1. INTRODUCTION

From available research documents, published reports and case studies, the typical level of hydrogen sulphide (H₂S) should be less than 1 ppm with the overall odour concentration of less than 2,000 OU/cu.m for most of the Sewage Pumping Stations (SPS) operating in Malaysia. (refer to Table 1)

However if the sewage collected and transferred to a SPS contains very high loading of oil and grease contaminants, the level of hydrogen sulphide can be exceptionally high. High levels of H₂S are dangerous and may lead to very severe health risks including the possibility of death.

Table 1. Some Odorous Compounds in Exhaust Air of a Typical Sewage Pump Stations.

Odorous Component	Detection Threshold (ppb)	Typical Level (ppb)	Odour Conc. (OU/cu.m)	Maximum Level (ppb)	Odour Conc. (OU/cu.m)
Acetaldehyde	67	30	< 1	100	< 2
Ammonia	17,000	100	< 1	2,000	< 1
Dimethyl Amine	340	20	< 1	50	< 1
Dimethyl Sulphide	1	50	50	100	100
Ethyl Mercaptan	0.3	50	165	100	330
Hydrogen Sulphide (H ₂ S)	0.5	1,000	2,000	30,000	60,000
Methylamine	4,700	50	< 1	100	< 1
Methyl Mercaptan	0.5	500	1,000	3,000	6,000
Skatole	1	50	50	N/A	N/A

2. ODOUR PROBLEM DEFINITION

Accurate Odour Problem Definition for a SPS or any other sewage collection or processing facilities shall include identifying odour generating sources followed by optimal containment of the identified sources.



Figure 1. Typical Sewage Pumping Station in Malaysia without Odour Control System



Figure 2. Olfactometric Measurement carried out in typical Malaysian Sewage Pumping Stations

From the odour concentrations measured at site by Olfactometry to MS 1963:2007 of numerous Sewage Pumping Stations installed and commissioned by Excel Air Engineering Sdn. Bhd., we recommend the Design of an Odour Control and Treatment System (OCTS) for a typical Sewage Pumping Station to be based on an Inlet Odour loading of 10,000 OU/cu.m.

For typical Sewage Pumping Stations in Malaysia, our standard BIORID Biofilter Odour Treatment Unit (OTU) Performance Efficiency is :

Ninety percent (90%) Odour Removal Efficiency for Inlet Odour load of 10,000 OU/cu.m

OR

Less than 1,000 OU/cu.m at Outlet Discharge for Inlet odour loads of less than 10,000 OU/cu.m.

3. CASE STUDY of a Not Typical Sewage Pumping Station in Malaysia with inlet sewage of very high odour levels and dangerous H₂S concentration

3.1. First Installation

3.1.1. Preliminaries

First look at an Odour Control System Project awarded to us for an existing Sewage Pumping Station



Figure 3. Initial photo of the existing Sewage Pumping Station for installation of our BIORID Odour Control System

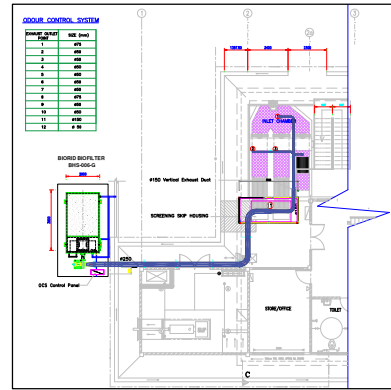


Figure 4. OCS Design Plan layout for a typical Sewage Pumping Station assumed applicable for this Project

3.1.2. First Installation at site

Closer look during onsite inspection for Installation



Figure 5. Onsite inspection showed the incoming sewage contain high oil and grease contents.

First Installation completed



Figure 6. Completed BIORID OCS of Containment System and OTU.

3.1.3. Measurements and Air flow balancing on completion of First Installation

On completion of installation works in end December 2010, air flow measurements were carried out on all exhaust points with air flow balancing on pressure basis to achieve the design flow rates at each extraction point. No odours were detected outside of the containment enclosures as all the exhaust odorous gases are contained and channeled into the BIORID Biofilter OTU with the treated air discharged to atmosphere.

On commissioning of the installed BIORID OCS, initial H_2S measurements at site by a hand held gas meter confirmed extraordinary high H_2S levels in the SPS incoming sewage (refer Figure 7).

The high acidity levels of both the BIORID Pre-scrubber and Biofilter effluent discharges at pH3 levels resulting from the extraordinary high H₂S concentration has severely corroded the concrete drain (refer Figure 8).



Figure 7. Hand held gas monitor detecting very high H₂S concentration above opening of wet well enclosure



Figure 8. Concrete drain badly corroded by acidic discharge from pre-scrubber and biofilter drain.

Sampling of the exhaust raw odorous gas and treated gas discharged at Outlet for H₂S and odour levels were carried out simultaneously with the collected gas samples sent to Lembaga Getah Malaysia (Olfactometry Laboratory approved by Jabatan Alam Sekitar) for determination of their odour levels by Olfactometry Analysis to MS1963:2007. (refer to Table 2 and Figure 9)

Table 2. Olfactometric Analysis to MS 1963:2007 was carried out on 24th May 2011.

Sample	Odour Concentration (OU/cu.m)	H ₂ S (ppm)
I1 Inlet raw gas before treatment	13,714	28.2
I2 Inlet raw gas before treatment	57,354	52.6
P1 Outlet treated gas	3,129	0.7
P2 Outlet treated gas	5,678	1.1

Figure 9. Olfactometric Measurement carried out after completion of installation

Fortunately, the hazardous and odorous sewage gases have been isolated from the SPS working environment by effective containment of these gases within the enclosures and covers of all the identified odour generating sources and exhausted to the inlet of the installed BIORID OTU.

3.1.4. Phase 1B Site Upgrading Works

Phase 1B Upgrading works were carried out on the installed BIORID OTU with addition of more organic biofilter media in the biofilter section increasing the effective biofiltration height by another 0.7 meter and topping up continuously fresh water into the pre-scrubber section for dilution of scrubbing water with continuous overflow draining back into the wet well.

On completion of Phase 1B Upgrading works, sampling of the exhaust raw odorous gas and treated gas discharged at OTU outlet for H₂S and odour levels were carried out simultaneously with the collected gas samples sent to Lembaga Getah Malaysia for determination of their odour levels by Olfactometry analysis to MS1963:2007 (refer to Figure 10 and Table 3).



Figure 10. H₂S levels measured in the incoming sewage at the channels, mechanical screens/skips and the inlet raw odorous gas to be abnormally high in some measurements recorded 200ppm H₂S which is the limit of the H₂S meter used.

Table 3. H₂S measurements taken at Odour Extraction Point and Inlet to BIORID Biofilter Odour Treatment Unit

		Ave. Velocity (m/s)	Volume (m ³ /h)	H ₂ S (ppm)
Main Duct - Inlet (Ø250mm)		4.12	727.19	170
Outlet at Exhaust BIORID Biofilter Plant				16
Point Extraction Velocities	Branch Duct mm	Ave. Velocity (m/s)	Volume (m ³ /h)	H ₂ S (ppm)
Point No.				
1	75	6.29	100.09	16 ppm
2	50	7.31	51.65	151 ppm
3	50	6.69	47.30	>200 ppm
4	50	7.13	50.38	73 ppm
5	50	5.72	40.43	>200 ppm
6	50	2.27	16.07	>200 ppm
7	50	4.45	31.46	200 ppm
8	75	6.01	95.64	75 ppm
9	50	5.20	36.78	56 ppm
10	50	4.76	33.63	80 ppm
12	50	3.56	25.16	10 ppm
Note : No Olfactometric Measurement carried out due to the high H ₂ S level.				

3.1.5. Health responses to High H₂S gases exposure

The danger and health risks are shown in Table 4 below.

Table 4. Hydrogen Sulphide and Health Hazards

Concentration (ppm)	Health Response
0.01 - 0.7	least detectable odour
3 - 5	offensive odour
10	eye irritation
20	irritation to mucous membranes and lungs
50 - 100	irritation of respiratory tract
150	nose nerve paralysis
200	headache, dizziness
500 - 600	nausea, excitement, unconsciousness
700 and above	FATAL

3.1.6. Identifying and Removal of Hazardous Chemicals before Odour Treatment

**TREAT ODOUR PROBLEMS for OFFENSIVE SMELL (ODOUR) ONLY
AFTER REMOVAL of IDENTIFIED HAZARDOUS CHEMICALS**

3.1.7. Recommended Solution

Problem : Remove H₂S from the extracted odorous gases to an acceptable level of below 5ppm H₂S before treating the remaining odorous gases by the existing BIORID Biofilter Plant.

Solution : Install an additional Wet Chemical Gas Scrubber to chemically treat and remove H₂S from the extracted odorous gases to an acceptable level before treatment by the existing BIORID Biofilter Plant.

3.2. Phase II Installation of Upgrading Works

3.2.1. Wet Chemical Gas Scrubber

The selected Wet Chemical Gas Scrubber to remove the H₂S from the extracted raw odorous gases is shown in Figure 11. The Phase II Overall OCS Design Plan layout is shown in Figure 12.

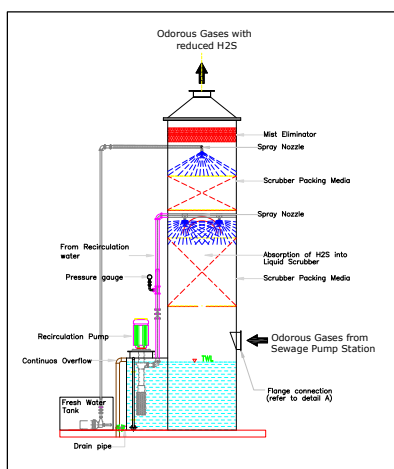


Figure 11. Selected Multiple Stage VCC Gas Scrubber for H₂S Removal

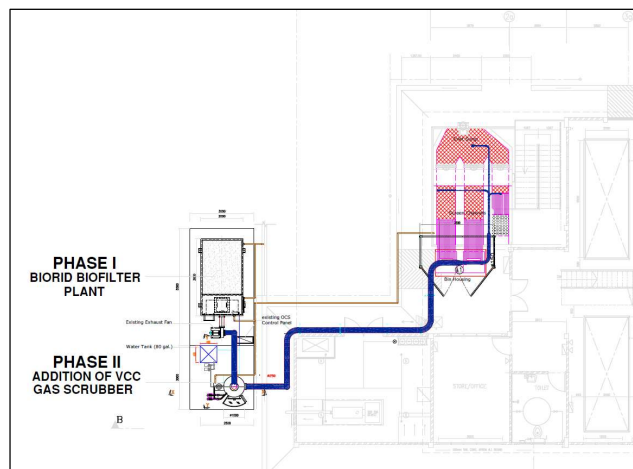


Figure 12. Phase II Overall OCS Design Layout

3.2.2. Phase II Installation at site



Figure 13. Completed Phase II Installation

3.2.3. High costs of Chemicals and resultant Waste Effluent Treatment of Wet Chemical Gas Scrubber

Before start-up of the installed Wet Chemical Gas Scrubber, the cost of neutralization by sodium hydroxide chemical scrubbing including the required treatment of the resultant chemical waste effluent were calculated to be too high. Therefore, it was decided to downgrade this Wet Chemical Gas Scrubber to be used only as a Water Gas Scrubber.

3.2.4. Measurements on completion of Phase II Upgrading Installation

On commissioning of the installed Upgraded OCTS of combined Water Gas Scrubber and BIORID Biofilter Plant in November 2011, sampling of the exhaust raw odorous gas, Water Gas Scrubber outlet and BIORID Biofilter final treated gas discharge for H₂S and odour levels were carried out simultaneously with the collected gas samples sent to Lembaga Getah Malaysia for determination of their odour levels by Olfactometry analysis to MS1963:2007. (refer to Table 5 and Figure 14)

Table 5. H₂S and Odour Measurements Of Odour Source, Local Exhaust Points, Raw Exhaust Gas Inlet to Water Gas Scrubber And Treated Exhaust Gas Outlet after BIORID Biofilter Plant From 14th Nov. To 16th Nov 2011

[illegible]

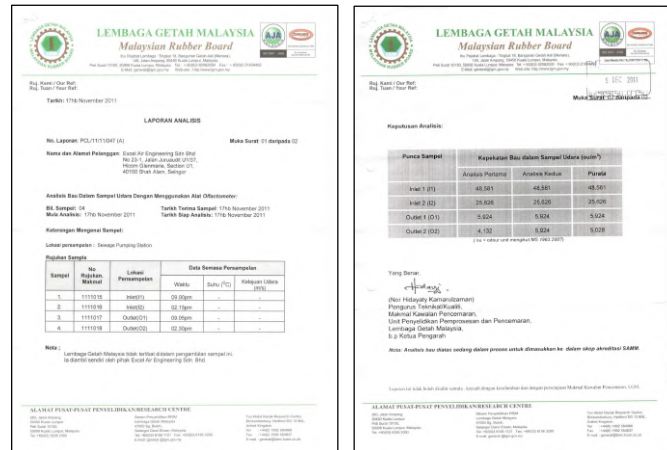


Figure 14. Olfactometric Measurement carried out after Phase II installation completion

3.2.5. Evaluation of Phase II Upgrading Installation

Now that the Wet Scrubber is using water as the scrubbing media, the level of H_2S at Scrubber Outlet is still very high ($>30\text{ppm } H_2S$). The existing BIORID Biofilter Plant has now been converted to a H_2S Removal Biofilter Plant and is unable to treat the remaining other odorous gases as shown clearly in Table 5 and Figure 14.

3.2.6. Recommended FINAL Solution

Problem : To further reduce the remaining odorous gases of $5,028 \text{ OU/cu.m}$ after the Phase II installation to below $< 1,000 \text{ OU/cu.m}$ as required before discharge to the atmosphere

Solution : Install an Additional second BIORID Biofilter Plant after the Exhaust Gas Outlet of the of the existing Phase II OCTS Installation of Water Gas Scrubber and first BIORID Biofilter Plant

3.3. Phase III Installation of Further Upgrading Works

3.3.1. Additional second BIORID Biofilter Plant

The additional second BIORID Biofilter Plant is be of closed top design and located after the Water Gas Scrubber and before the existing open top BIORID Biofilter Plant. (Refer Figures 15 and 16)

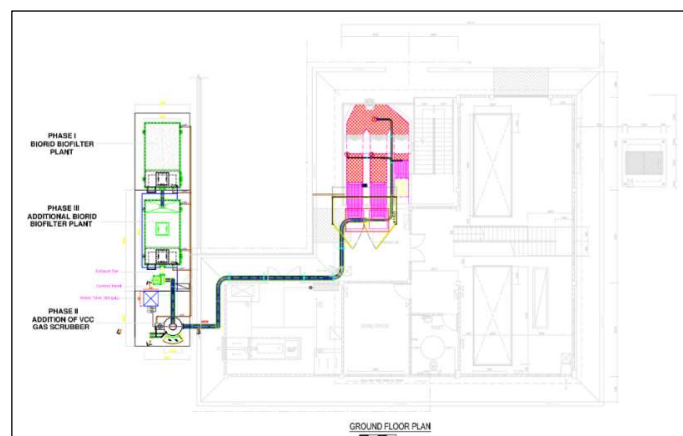


Figure 15. Phase III Overall OCS Design Plan layout

3.3.2. Phase III Installation at site



Figure 16. Completed Phase III Installation

3.3.3. Measurement on completion of Phase III Further Upgrading Installation

On commissioning of the Phase III Further Upgrading Installation in January 2013, sampling of the final treated odorous gas discharge for H_2S and odour levels were carried out at site with the collected gas samples sent to Lembaga Getah Malaysia for determination of their odour levels by Olfactometry analysis to MS1963:2007. (refer to Figure 17)

Figure 17. Olfactometric Measurement carried out after commissioning of Phase III Installation

3.3.4. Evaluation of Phase III Upgrading Installation

Referring to Figure 17, the installation of the additional second BIORID Biofilter OTU has reduced the Phase II treated odour level of 5,028 OU/cu.m (as shown in Treated Exhaust Gas OULET in Table 6) to 720 OU/cu.m below the emission odour limit of 1,000 OU/cu.m as required by the Sewage Pumping Station Owner.

3.3.5. Summary of Results for all three of installations

The results of Phase III Further Upgrading Installation is compared to the earlier results of Phase II Upgrading Installation and First Installation is shown in Table 6.

Table 6. Summary of Measurement Result taken for all 3 Phases of OCTS Installations, From May 2011 to January 2013

Item	Date & Time of Site Sampling	24-May-11		11-Aug-11		15-Nov-11				16-Nov-11		30-Jan-13	
		Phase 1A Biofilter Plant only		Phase 1B Upgrade Biofilter Plant		Phase II Biofilter Plant with additional 2 stage VCC Water Scrubber						Phase III Additional Biofilter Plan	
	Description	12:20 PM	12:40 PM	10:55 AM	1:50 PM	11:40 AM	1:30 PM	7:40 PM	9:00 PM	10:30 AM	2:15 PM	9:50 AM	10:50 PM
(A)	H ₂ S Concentration (ppm)												
1	Raw Exhaust Gases INLET	28.2	52.6	143	170.0	100.0	94.0	118.0	66.0	73.0	53.0	46.0	86.0
2	Treated Exhaust Gases OUTLET	0.7	1.1	11	16.0	5.0	5.0	1.0	<1.0	0.0	0.0	0.0	0.0
(B)	Odour Concentration (OU/cu.m)												
1	Raw Exhaust Gases INLET	13,714	57,354	(1)	(1)	(2)	(2)	(2)	48,581	(2)	25,626	(2)	(1)
2	Treated Exhaust Gases OUTLET	3,129	5,678	(1)	(1)	(2)	(2)	(2)	5,924	(2)	5,028	(2)	720
Notes : 1. Due yo excessive H2S concentration measured, olfactometric analysis were not carried out. 2. Olfactometric analysis carried out only for 1 night time sampling and 1 day time sampling													

3.4. CONCLUSION

From the Summary of Results in Table 6 and the actual site conditions in this Case Study, the requirements stated below must be strictly followed for all future Odour Control and Treatment Systems to be installed in a Sewage Pumping Station, Sewage Treatment Plant or any other Sewage Handling and Processing Facility.

1. Accurately define the actual odour Problem with focus on hazardous chemicals such as hydrogen sulphide, ammonia, methane, sulphur dioxide and others before treating the remaining odorous gases to below the allowable odour concentration level.
2. Optimal containment of identified odour generating sources is critical to isolate the odorous gases from the surrounding environment especially to prevent direct exposure to persons working in the facility.
3. Where practical, treat the defined odour problem at raw sewage collecting sources before inlet collection point at the facility. In this case study, the oils and grease contents should be removed or reduced from the incoming sewage before the Sewage Pumping Station.
4. Where specified or due to abnormally identified hazardous chemicals, combination of several odour treatment technologies should be considered.
5. The measured results show that a Biofiltration treatment system with proven design and successfully commissioned installations, is able to remove H₂S effectively
6. To be considered cost-effective, OCTS operation and maintenance costs must be carefully evaluated before selecting an OTU to be installed.

From the data collected at site and measurement results, it is reasonable to conclude that the **Better Solution** to treat sewage odorous gases of similar extraordinary high H₂S would be a **Combination** of one **Closed top Biofilter** and one **Open top Biofilter Odour Treatment System**.

4. ACKNOWLEDGMENTS

This work was carried out in compliance to the requirements of the Sewage Pumping Station Owner.

5. REFERENCES

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